





Diagnosis of plantwide oscillations: A harmonics analysis approach

Nahid Sanzida ^{1,*}, M. A. A. Shoukat Choudhury ²

^{1, 2} Department of Chemical Engineering, Bangladesh University of Engineering & Technology, Dhaka, Bangladesh

Index Terms: Plantwide Oscillations Root Cause Diagnosis Nonlinearity Harmonics

Received: 15 July 2015 Accepted: 13 November2015 Published: 15 October 2015 **Abstract**—Highly complex and integrated modern chemical process plants are susceptible to disturbances propagate throughout the plant from one unit to other interconnected units and create plantwide oscillations. These persisting oscillations are originated due to various faults such as sensor faults, valve faults, process faults, and controller tuning faults. A fundamental frequency and its harmonics can characterize these types of nonlinear faults. This paper demonstrates a novel data-driven off-line time-domain method to identify the root cause of plantwide or unit-wide disturbances to troubleshoot plantwide disturbances using harmonics analysis. The successful application of the proposed method has been demonstrated through simulated data.

© 2015 TAF Publishing. All rights reserved

I. INTRODUCTION

It is obvious that when an oscillation is generated in a particular part in a highly complex and integrated modern chemical process plants, it then propagates throughout the whole plant or a group of interconnected units. These oscillations are termed as plantwide or unitwide oscillation(s) which ultimately pose a large threat on product quality, running cost and profitability because production and throughput may have to back away from their optimum settings to accommodate process variability [1].

Thus, it is important for process control engineers to

detect and diagnose the causes of oscillations or disturbances in a chemical process operation as soon as possible [2], [3]. Over the last few years, some studies

were carried out to detect plantwide oscillations [4], [5] and to group the similar oscillations together. For the detection of oscillations in process measurements and identify signals with common oscillatory behavior, the use of spectral principal component analysis (PCA) [6] or autocorrelation function (ACF) [7] is suggested. [8] have proposed a technique that takes into account the interaction between the control loops. [9] introduced a new index called power spectral correlation index (PSCI) which is the correlation between the power spectra of two different measurements.

They proposed the use of PSCMAP (Power spectral

* Corresponding author: Nahid Sanzida E-mail: nahidsanzida@che.buet.ac.bd



correlation map) to automatically re-arrange and group variables together, which oscillate at a common frequency. However, after the detection of plantwide oscillation, the next step is the diagnosis of its root-cause. Recently there appeared a few papers that described a few techniques to perform root-cause diagnosis of plant-wide oscillation [9], [10], [11], [12], [13]. [6] Proposed a new procedure based on the spectral envelope method for detection and diagnosis of common oscillation(s). This paper demonstrates a novel data driven off-line time domain method to troubleshoot plantwide disturbances using harmonic analysis.

A. Oscillations and Harmonics

It is observed that nonlinearity induced oscillatory signals generally contain a fundamental frequency and its harmonics. A very common cause for oscillation is the presence of nonlinearity such as a valve stiction which often results in square-like waves in the controlled variable [15]

Figure 1 demonstrates the time series data and corresponding power spectra for a sticky valve. The time trend is almost rectangular and the power spectra give peaks at the normalized frequency of 0.0078, 0.024 and 0.039. Here, 0.0078 is the fundamental frequency and 0.024 and 0.039 are the third and fifth harmonics respectively. According to Fourier series any signal can be represented as a summation of sinusoids. Therefore, any time series y(t), where t \in R can be represented as,

$$y(t) = \sum_{i=0}^{\infty} A_i \cos(\lambda_i t + \phi_i)$$
(1)

For a signal containing harmonics, Equation (1) takes the following form:

$$y(t) = \sum_{i=0}^{M} A_{i}\cos(i * \lambda t + \phi_{i}) + \varepsilon(t)$$
(2)



Fig. 1. Time series data and the power spectra for a sticky

valve.

Where, λ is the fundamental frequency. The general approach is to estimate the amplitudes, frequencies and phases for each term of Equation (2) and then examine the relationships among the frequencies to identify the presence of harmonics in the signal. [4] Suggested that it suffices to write the above expression only up to fifth harmonics for useful application of the analysis of chemical process data.

B. Total Harmonic Content (THC)

A new index called the Total Harmonic Content (THC) can be defined by the following expression of Equation 3, $THC = n \times WHM$ (3)

Where, *n* is the number of harmonics found and *WHM* is the Weighted Harmonic Mean. *WHM* is defined as,

$$WHM = \frac{\sum_{i=1}^{M} w_i}{\sum_{i=1}^{M} w_i / A_i}$$
(4)

where w_i is weights and is defined as $w_i = i / \sum_{i=1}^{M} i$. Due to the low-pass filtering effect of the chemical processes, the higher harmonics get filtered out gradually as the signal propagates away from the source or the root cause. Hence, more weights are given to the higher harmonics.

For plantwide oscillation(s) detection, the amplitudes, frequencies and phases of first five terms of equation (2) are estimated for time series data of each tag. Tags or variables having the same fundamental frequency and harmonics (if any) are identified. Weighted harmonic mean is calculated using amplitudes whose frequencies are in harmonics and multiplied by number of harmonics present. After calculating the THCs using equation (3), the variables are ranked according to the descending order of THC. The possibility of being the root cause increases with the increase of the value of THC.

II. CASE STUDY

C. Simulation Example

This simulation example involves a large, industrially relevant system of vinyl acetate monomer (VAc) manufacturing process. [14] Developed the Nonlinear Dynamic Model of this VAc process in MatLab which is freely available from the authors' website.

In the VAc process, there are 10 basic unit operations, which include a vaporizer, a catalytic plug flow reactor, a feed-effluent heat exchanger (FEHE), a separator, a gas



compressor, an absorber, a carbon dioxide (CO₂) removal system, a gas removal system, a tank for the liquid recycle stream and an azeotropic distillation column with a decanter. There are seven chemical components in the VAc process. Ethylene (C₂H₄), pure oxygen (O₂), and acetic acid (HAc) are converted into the vinyl acetate (VAc) product, and water (H₂O) and carbon dioxide (CO₂) are byproducts. An inert, ethane (C₂H₆), enters with the fresh C₂H₄ feed stream. For details, refer to [1]. Figure 2 shows a simplified schematic of the Vinyl Acetate Process with the locations of the manipulated variables.



Fig. 2. VAc process flowsheet [1].

In order to create plantwide oscillations disturbance, valve stiction was introduced to control loops 9 and 14, independently. Valve stiction was introduced using Choudhury's stiction model [3]. To create limit cycle oscillations. The oscillation then propagate to the other control loops and eventually to the whole plant or some part of the plant.

In loop 9, the controlled variable is the separator temperature and the manipulated variable is the separator coolant valve corresponding to the cooling water flow rate for the separator jacket. After the process reached steady state, 5% stiction (where S = J) was introduced in the manipulated variable coolant valve. Simulation data set consisted of 2000 minutes of data with a sampling time of 15 seconds; therefore, each variable has 8000 observations. The last 1024 data points were used in this analysis in order to avoid transient behavior due to the sudden introduction of stiction.



Fig. 3. Time trends and power spectra for the VAc process



variables, applied stiction in loop 9 is 5%.

Fig. 4. THC values for the VAc process variables for 5% stiction applied in loop 9.

Figure 3 shows the time trends and power spectra which indicates that the variables 1, 2, 4, 5, 6, 7, 8, 9, 11, 12, 14, 21 and 22 are oscillating together. The high density plot reveals that they are oscillating at a normalized frequency of 0.0505.

Table 1 shows the harmonic analysis of the simulated data. The algorithm correctly identifies the presence of sinusoids in the signal. Five sinusoids are estimated for each signal. Total Harmonic Content (THC) was calculated for these variables. The maximum THC corresponds to tag 9 indicating the source or root-cause of the propagated oscillation because stiction was introduced in this variable during simulation. Figure 4 shows the calculated THC values against the variable or tag number.

D. An Industrial Example-Application to a Refinery Data Set

The proposed method was applied to a benchmark industrial data set for plantwide oscillations study appeared in the literature such as [9]-[10].

The data set, courtesy of a SE Asian Refinery, consists of 512 samples of 37 measurements sampled at 1 min interval. It comprises measurements of temperature, flow, pressure and level loop along with some composition measurements. Figure 5 depicts the time trends of the controller errors and the corresponding power spectra.

The calculated THC values are plotted against the tag number in Figure 6. The highest THC value corresponds to the tag no. 34, which is the first candidate for the possible



root-cause of this plantwide oscillation.

Tinie Trends	Power Spectra							
2 prove and and a strange and the second second and the second se	FC-BOOB PV							
No. of the second se	TURCON PV							
38 mon when the the work of the work of the	ALMORD PV							
SALAMANANANANANANANANANANANANANANANA	FITESO4 PV	CLERCE DO	11000					
mighter server and the astrony to the server of the server	PC763018 PV							
THE RE-PROPERTY AND ADDRESS OF THE PROPERTY ADDRESS OF	PC28XIZ PV							
Manhamman Manhamman .	#C35018 PV		11					
30 Roman Service and an extension service and an extension of the service of the	FC38017 PV							
25 Titler of Macan Confidence and share? All all papers of the an	PC79012 PV							
28 A MARINA M	PC28011 PV		11111					
27 martineter and a second survey of the second sec	PC28008 PV							
28 Margar James Margar Margaret Margaret	ECTION PV							
HAR BUNG MARKER MARKEN MARKEN AND AND	FC29004 PV							
and have an experimental in a marked of the	PC1600 PV		1.1					
23 Million City, edu Alland Maria and Antonio Maria Maria Maria	PC78001 PV							
22 is sector and an international funder	ADDING PUT							
the standard at a set	ADSOLS PV							
Without address a dd and any address and and	Attended my		1.					
10 to a state which all a said many and a said	ADDVIS PV							
and a second of the Association	LC TROOP PU							
17 march & A Company & Company	L CTRODE PV							
10 Mary and an and and a should be and and and and	LC TROOT BY		8					
an addition of the second of the second of the second of the	LOTROP PU							
HI CONTRACTOR AND	CONTRACTOR PARTY							
11 AAA CEBACTERTON TARA CANTAGERTON CON	Lothersh Par							
- and the state of the state of the	LC35003 PV	1						
13 Marsh Marshan manual marshan	POISOR PV							
188.84.44.44.44.44.44.44.44.44.44.44.44.4	PC30064 PV							
المروانية والمانية والمرور والالا ومراجعة معاركة والمراجع	PCTROOP P's							
+ was within many approximation within	PC78036 PV	11111	1.11311					
7 - Hard Monor at me all the bridge all the	PCTRODE PV							
+ Land and and marked through a stranger and a seattle	PC30011 PV	11116						
	TC/10096 PV							
a hastron and a source the mary market	TOTAL PLANT							
133444444444444444444444444444444444444	TC3064 PV							
2 1000000000000000000000000000000000000	TC1803 PV							
1 Mar - MAR - MAR AND AND AND - MAR - MAR - MAR - MAR	TC28013 PV							
1 all a day a stand de day de day a	Contraction of the							
A States A	2	0.01	0.1					

Fig. 5. Time trends and power spectra for the South-East Asia refinery data set.

From these figures, it can be found that the tags 2, 3, 4, 8, 9, 10, 11, 13, 15, 16, 17, 19, 20, 24, 25, 28, 33 and 34 are oscillating together with a common frequency of 0.0605 or 17 samples/cycle approximately. All data corresponding to the variables with the common frequency were first normalized so that they had zero mean and unit variance. Then the amplitudes, frequencies and phases for first five sinusoids were estimated and THCs were calculated for these variables.



Fig. 6. Total harmonic contents (THC) results for SEA refinery data set.

In real plant investigation if this tag is not found to be the root cause, then the tag corresponding to next highest value of THC should be investigated. For this case, earlier studies [9], [10] and [11] found tag 34 as the root-cause. Therefore, the proposed THC index correctly detected the root-cause of this plantwide oscillation.

III. CONCLUSION AND FUTURE WORK

In this paper a new index called THC (Total Harmonic

Content) is introduced to troubleshoot plantwide oscillation(s). Through simulation and industrial data analysis case studies, it has been shown that THC is an effective tool for isolating the root cause of plantwide oscillation(s). The method can be automated to facilitate troubleshooting of plantwide oscillation.

ACKNOWLEDGMENT

We acknowledge Bangladesh University of Engineering and Technology (BUET), Dhaka, Bangladesh, for technical support and funding for this research.

REFERENCES

- R. Chen, K. Dave, T. McAvoy and M. Luyben, M. A nonlinear dynamic model of a vinyl acetate process. Indian *Engineering Chemical Resources*, vol. 42, no. 20, pp. 4478 - 4487. 2003. DOI: 10.1021/ie020859k
- [2] M. A. S. Choudhury, M. A. Karim, S. Barua and N. Sanzida, "Root cause diagnosis of plantwide disturbance using harmonic analysis," in *Preprints of ADCHEM 2009*, (pp. 305- 309), Istanbul, Turkey.
- [3] M. A. A. S. Choudhur, S. L. Shah and N. F. Thornhill, Diagnosis of Process Nonlinearities and Valve Stiction-Data Driven Approaches. Springer Berlin Heidelberg, 2008.
- [4] M. A. A. S. Choudhury, V. Kariwala, N. Thornhill, H. Douke, S. Shah, H. Takadac and J. Forbes, "Detection and diagnosis of plantwide oscillations," *Canadian Journal of Chemical Engineering*, vol. 85, no. 2, pp. 208–219, 2007. DOI: 10.1002/cjce.5450850209
- [5] A. Horch, V. Hegre, K. Hilmen, H. Melbø, L. Benabbas, S. Pistikopoulos, N. F. Thornhill and N. Bonavita. (n.d). *Root cause-University and industry co-operation*. [Online]. Available
 https://library.e.abb.com/public/f622752d28bc2afe8
 525704c006ec6fc/RootCause_HorchTornhillBonavita. pdf, date accessed July 25, 2015.
- [6] H. Jiang, M. A. A. S. Choudhury and S. L. Shah, "Detection and diagnosis of plantwide oscillations from industrial data using the spectral envelope method," *Journal of Process Control*, vol. 17, no. 2, pp. 143–155, 2007. DOI: 10.1016/j.jprocont.2006.09.006
- M. A. Paulonis and J. W. Cox, "A practical approach for large-scale controller performance assessment, diagnosis and improvement," *Journal of Process Control*, vol. 13, no. 2, pp.155–68, 2003. DOI: 10.1016/S0959-1524(02)00018-5
- [8] S. J. Qin, "Control performance monitoring-A review and assessment," *Computers and Chemical*

33

Engineering, vol. 23, no. 2, pp. 173-186, 1998. DOI:10.1016/S0098-1354(98)00259-2

- [9] A. Tangirala, S. Shah and N. Thornhill, "PSCMAP: A of Process Control, vol. 15, no. 8, pp. 931-941, 2005. **DOI:** 10.1016/j.jprocont.2005.01.005
- [10] A. Tangirala, J. Kanodia and S. L. Shah, "Non-negative plantwide oscillations," Industrial & Engineering Chemistry Research, vol. 46, no. 3, pp. 80 -817, 2007. DOI: 10.1021/ie0602299
- [11] N. F. Thornhill, S. L. Shah, B. Huang and A. Vishnubhotla, "Spectral principal component analysis of dynamic process data," Control Engineering Practice, vol. 10, pp. 833-846, 2002. DOI: 10.1016/S0967-0661(02)00035-7
- [12] N. F. Thornhill, B. Huang and H. Zhang, "Detection of

multiple oscillations in control loops," Journal of Process Control, vol. 13, no. 1, pp. 91-100, 2003. DOI: 10.1016/S0959-1524(02)00007-0

- new tool for plantwide oscillation detection," Journal [13] C. Xia and J. Howell, "Loop status monitoring and fault localization," Journal of Process Control, vol. 13, no. 7, DOI: 10.1016/S0959pp. 679-689, 2003. 1524(02)00123-3
- matrix factorization for detection and diagnosis of [14] X. Zang and J. Howell, "Isolating the root cause of propagated oscillations in process plants," International Journal of Adaptive Control and Signal Processing, vol. 19, no. 4, pp. 247-265, 2005. DOI: 10.1002/acs.860
 - [15] X. Zang and J. Howell, "Isolating the source of wholeplant oscillations through bi-amplitude ratio analysis," Control Engineering Practice, vol. 15, no. 1, pp. 69-76, 2007.

DOI: 10.1016/j.conengprac.2006.03.006

Appendix

MV	λ1	λ2	λ3	λ4	λ5	A ₁	A ₂	A ₃	A ₄	A ₅	\$ 1	\$ 2	\$ 3	\$ 4	\$ 5	λ_1/λ_1	λ_2/λ_1	λ ₃ /λ ₁	λ4/λ1	λ_5/λ_1	RESS	THC
1	0.317	0.951	1.585	2.219	2.853	1.339	0.309	0.169	0.114	0.083	-0.69	2.812	0.856	-0.91	-2.63	1.000	3.000	5.000	7.000	9.000	30.8	0.450
2	0.317	0.951	1.585	2.219	2.853	1.383	0.266	0.101	0.051	0.029	-2.44	1.366	-0.50	-2.24	2.397	1.000	3.000	5.000	7.000	9.000	1.8	0.293
3	0.006	0.317	0.012	0.018	0.043	1.004	0.968	0.237	0.073	0.033	-0.17	2.731	0.479	0.874	1.374	1.000	50.00	1.891	2.846	6.711	2.7	
4	0.317	0.951	1.585	2.219	0.323	1.401	0.161	0.058	0.029	0.024	0.123	-2.13	2.376	0.692	-1.61	1.000	3.000	5.000	7.000	1.019	1.2	0.136
5	0.317	0.951	1.585	2.219	2.853	1.218	0.389	0.235	0.168	0.130	-1.00	2.952	1.142	-0.46	-2.01	1.000	3.000	5.000	7.000	9.000	135.4	0.603
6	0.317	0.951	1.585	2.219	0.323	1.399	0.184	0.067	0.033	0.025	-2.60	1.229	-0.66	-2.43	1.934	1.000	3.000	5.000	7.000	1.019	1.2	0.151
7	0.317	0.951	1.585	2.219	0.323	1.401	0.181	0.057	0.025	0.026	-2.37	0.709	-1.38	2.947	2.175	1.000	3.000	5.000	7.000	1.019	0.9	0.140
8	0.317	0.951	1.585	2.219	0.323	1.402	0.150	0.052	0.025	0.026	-0.76	-2.44	2.196	0.567	-2.50	1.000	3.000	5.000	7.000	1.019	0.9	0.129
9	0.317	0.951	1.585	2.220	2.854	1.272	0.423	0.252	0.178	0.137	-2.33	2.400	0.848	-0.69	-2.22	1.000	3.000	5.000	7.000	9.000	45.0	0.649
10	0.004	0.012	0.021	0.029	0.038	1.316	0.445	0.264	0.177	0.137	-3.08	0.600	-2.44	0.951	-1.99	1.000	2.854	4.858	6.838	8.735	36.0	
11	0.317	0.951	1.585	2.219	0.323	1.387	0.245	0.085	0.037	0.024	-3.01	0.791	-1.28	3.055	1.558	1.000	3.000	5.000	7.000	1.019	1.2	0.177
12	0.317	0.951	0.323	0.311	1.585	1.412	0.067	0.026	0.025	0.009	0.613	-2.90	-1.14	-0.98	1.160	1.000	3.000	1.019	0.982	5.000	0.3	0.033
13	0.004	0.030	0.009	0.063	0.093	1.254	0.231	0.242	0.101	0.071	2.791	2.051	-3.04	-1.73	1.769	1.000	7.966	2.402	16.54	24.55	10.5	
14	0.317	0.323	0.311	0.951	0.029	1.411	0.025	0.025	0.018	0.015	0.059	-1.68	-1.61	-2.98	-0.75	1.000	1.020	0.982	3.000	0.090	0.5	0.024
15	0.004	0.025	0.009	0.078	0.052	1.241	0.236	0.238	0.086	0.127	2.823	2.336	-2.96	2.133	-1.10	1.000	6.474	2.399	20.46	13.55	14.8	
16	0.006	0.012	0.017	0.029	0.023	1.404	0.346	0.134	0.091	0.093	3.104	-3.09	-3.03	2.895	3.065	1.000	1.902	2.719	4.547	3.630	3.0	
17	0.007	0.014	0.024	0.030	0.042	1.245	0.516	0.299	0.203	0.140	2.886	0.549	2.713	1.675	-3.12	1.000	1.971	3.407	4.190	5.909	31.6	1
18	0.007	0.011	0.004	0.020	0.025	0.927	0.382	0.798	0.181	0.082	-2.71	2.195	-2.50	-2.48	2.587	1.000	1.581	0.611	2.840	3.556	10.7	
19	0.317	0.951	0.323	0.311	1.585	1.409	0.085	0.026	0.024	0.022	2.335	-1.29	0.610	0.687	2.766	1.000	3.000	1.019	0.982	5.000	0.4	0.064
20	0.006	0.157	0.314	0.471	0.012	0.944	0.807	0.407	0.272	0.168	-0.14	1.508	1.434	1.323	0.049	1.000	24.41	48.82	73.25	1.926	102.4	
21	0.317	0.006	0.951	0.157	0.323	1.411	0.052	0.043	0.039	0.028	-1.55	-0.02	-1.33	-0.14	3.088	1.000	0.020	3.000	0.496	1.018	0.5	
22	0.317	0.951	0.006	1.585	0.323	1.408	0.099	0.037	0.028	0.026	-1.15	-2.27	0.144	2.112	-2.80	1.000	3.000	0.020	5.000	1.019	1.0	
23	0.317	0.157	0.951	0.323	0.311	1.411	0.069	0.033	0.028	0.017	-2.63	-2.19	2.428	2.162	2.553	1.000	0.495	3.000	1.018	0.980	0.3	
24	0.006	0.317	0.012	0.018	0.024	1.110	0.853	0.241	0.091	0.046	-0.14	-2.75	0.449	0.587	0.446	1.000	50.19	1.870	2.831	3.842	2.1	
25	0.317	0.006	0.012	0.323	0.311	1.395	0.214	0.046	0.027	0.024	1.083	2.980	-2.69	-0.70	-0.34	1.000	0.020	0.038	1.019	0.982	0.7	
26	0.004	0.012	0.021	0.029	0.038	1.316	0.445	0.264	0.177	0.137	0.060	-2.54	0.701	-2.19	1.148	1.000	2.854	4,858	6.838	8,735	36.0	

